

Solenoid valves Type EVR 2 to 40

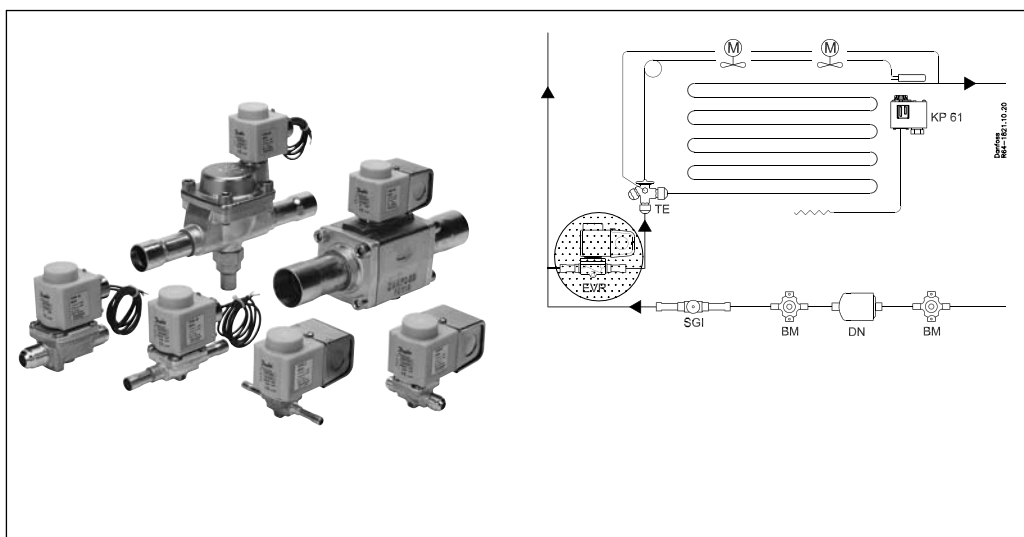
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Metric conversions

- 1 psi = 0.07 bar
- $5/9 (t_1^{\circ}\text{F} - 32) = t_2^{\circ}\text{C}$
- 1 ton = 3.5 kW
- 1 in. = 25.4 mm
- 1 ft = 0.3 m
- 1 lb = 0.454 kg
- 1 oz = 28.35
- US gal/min = 0.86 m³/h

Introduction



This leaflet presents a newly extended program of Danfoss solenoid valves, type EVR. The program includes a new coil design, type GP, with a quick and easy “clip-on” system.

EVR is a direct or servo operated solenoid valve for liquid, suction, and hot gas lines using fluorinated refrigerants.

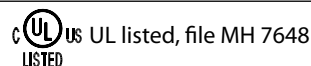
EVR valves are supplied as separate components; valve body and coil, if required, can be ordered completely.

Features

- A complete range of solenoid valves for refrigeration, freezing and air conditioning systems
- Normally closed (NC) and normally open (NO) versions available
- AC and DC coils are interchangeable on all valve body versions
- Use with any fluorinated refrigerant
- Designed for media temperatures up to 220°F
- Flare connections up to 5/8 in.
- Solder connections up to 2-1/8 in.
- Solder versions have extended connections; there is no need to dismantle the valve when soldering

Approvals

Note:
These approvals are only recognized when one of the EVR series of solenoid valves found in this leaflet is combined with a GP general purpose coil.



Metric conversions
 $5/9 (t_1^{\circ}F - 32) = t_2^{\circ}C$
 1 in. = 25.4 mm

Technical data
Refrigerant

R 22, R 134a, R 404A, R 507 etc.

Maximum working pressure

EVR 2 to 10: MWP = 500 psig

EVR 15 to 22: MWP = 460 psig

EVR 25 to 40: MWP = 460 psig

Temperature of medium

- 40 to 220°F

Maximum 265°F during defrosting

Enclosure of coil

NEMA 2 or NEMA 4

Valve type	Opening differential pressure Δp psi			Medium temperature °F	Maximum working pressure MWP psig	Cv value ¹⁾ gal/min
	Minimum	Maximum (= MOPD) liquid ²⁾				
		AC	DC			
EVR 2	0.0	350	260	- 40 to 220	655	0.19
EVR 3	0.0	300	260	- 40 to 220	655	0.32
EVR 4	0.7	300	260	- 40 to 220	500	0.66
EVR 6	0.7	300	260 ³⁾	- 40 to 220	500	0.93
EVR 8	0.7	300	260	- 40 to 220	500	1.3
EVR 10	0.7	300	260 ³⁾	- 40 to 220	500	2.2
EVR 15	0.7	300	260 ³⁾	- 40 to 220	500	3.0
EVR 18	0.7	300	260	- 40 to 220	500	3.9
EVR 20	0.7	300 ⁴⁾	190	- 40 to 220	500	5.8
EVR 22	0.7	300 ⁴⁾	190	- 40 to 220	500	6.9
EVR 25	1.0	300	260	- 40 to 220	460	12.0
EVR 32	1.0	300	260	- 40 to 220	460	18.0
EVR 40	1.0	300	260	- 40 to 220	460	29.0

¹⁾ C_v value is the water flow in gal/min at a pressure drop across valve $\Delta p = 1$ psi, $\rho = 10$ lbs/gal

²⁾ MOPD for media in gas form is approximately 14 psi greater

³⁾ EVR (NO): 300 psig

⁴⁾ EVR (NO): 275 psig

Valve type	Rated capacity ¹⁾ tons								
	Liquid			Suction vapor			Hot gas		
	R 22	R 134a	R 404A/R 507	R 22	R 134a	R 404A/R 507	R 22	R 134a	R 404A/R 507
EVR 2	1.17	0.89	0.80	0.10	0.07	0.09	0.22	0.18	0.17
EVR 3	2.03	1.55	1.40	0.17	0.13	0.15	0.38	0.31	0.30
EVR 4	4.15	3.16	2.86	0.34	0.26	0.30	0.77	0.63	0.62
EVR 6	5.83	4.43	4.01	0.48	0.37	0.43	1.08	0.88	0.87
EVR 8	8.01	6.09	5.52	0.66	0.51	0.58	1.49	1.21	1.19
EVR 10	13.8	10.5	9.53	1.15	0.88	1.01	2.57	2.10	2.06
EVR 15	18.9	14.4	13.0	1.57	1.20	1.38	3.52	2.87	2.82
EVR 18	24.6	18.7	17.0	2.04	1.56	1.80	4.57	3.73	3.67
EVR 20	36.4	27.7	25.1	3.02	2.31	2.66	6.76	5.51	5.43
EVR 22	43.7	33.3	30.1	3.62	2.78	3.19	8.11	6.62	6.52
EVR 25	72.8	55.4	50.2	6.04	4.63	5.32	13.5	11.0	10.9
EVR 32	116.5	88.7	80.3	9.66	7.40	8.51	21.6	17.7	17.4
EVR 40	182.0	138.5	125.4	16.1	11.6	13.3	33.8	27.6	27.2

Metric conversions

1 psi = 0.07 bar

 $5/9 (t_1^{\circ}\text{F} - 32) = t_2^{\circ}\text{C}$

1 ton = 3.5 kW

1 in. = 25.4 mm

 US gal/min = 0.86 m³/h

¹⁾ Rated liquid and suction vapor capacity are based on:

 Evaporating temperature $t_e = 40^{\circ}\text{F}$

 Liquid temperature ahead of valve $t_l = 100^{\circ}\text{F}$

 Pressure drop Δp across valve

 - with liquid $\Delta p = 2$ psi for R 134a

 $\Delta p = 3$ psi for R 22, R 404A and R 507

 - with suction vapor $\Delta p = 1$ psi

Rated hot gas capacity is based on:

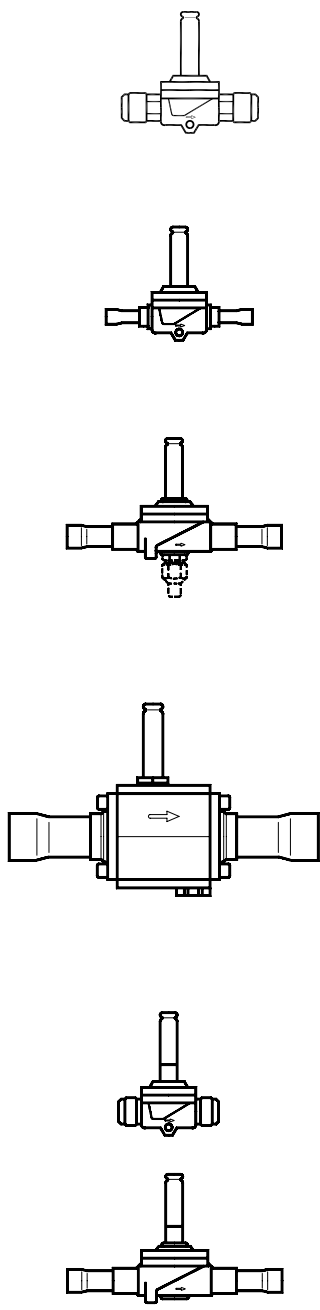
 Condensing temperature $t_c = 100^{\circ}\text{F}$

 Hot gas temperature $t_h = 140^{\circ}\text{F}$

 Pressure drop across valve $\Delta p = 2$ psi

Ordering

Separate valve bodies for EVR, normally closed (NC)



Type	Rated capacity R 22 (liquid) tons	Conne- ction in.	Port size in.	C _v value gal/min	Code nos. valve body excl. coil		
					Flare		Solder ODF
					Without manual stem in.	With manual stem in.	without manual stem in.
EVR 2	1.17	1/4	3/32	0.19	32F8058		32F7100
EVR 3	2.03	1/4	1/8	0.32	32F8106		32F7105
EVR 3	2.03	3/8	1/8	0.32	32F8115		32F1157
EVR 4	4.15	3/8	5/32	0.66	32F8087	32F7172	32F7110
EVR 4	4.15	1/2	5/32	0.66	32F8089		
EVR 6	5.83	3/8	15/64	0.93	32F8071	32F7116	32F7115
EVR 6	5.83	1/2	15/64	0.93		32F7144	32F1162
EVR 6	5.83	5/8	15/64	0.93			32F7117
EVR 8	8.01	3/8	5/16	1.3			32F7120
EVR 8	8.01	1/2	5/16	1.3		032F7148	32F7121
EVR 8	8.01	5/8	5/16	1.3			32F7122
EVR 10	13.8	3/8	3/8	2.2			32F7125
EVR 10	13.8	1/2	3/8	2.2		32F1188	32F1166
EVR 10	13.8	5/8	3/8	2.2		32F7149	32F1168
EVR 15	18.9	5/8	9/16	3.0		32F1172	32F1171
EVR 15	18.9	7/8	9/16	3.0			32F7130
EVR 18	24.6	7/8	19/32	3.9		32F1004	
EVR 18	24.6	1 1/8	19/32	3.9			
EVR 20	36.4	7/8	7/8	5.8		32F1177	32F1176
EVR 20	36.4	1 1/8	7/8	5.8		32F2272	
EVR 22	43.7	1 1/8	15/16	6.9		32F7137	32F7145
EVR 22	43.7	1 3/8	150/16	6.9			32F7146
EVR 25	72.8	1 1/8	1	12.0		32F1190	32F1189
EVR 25	72.8	1 3/8	1	12.0		32F1194	32F1193
EVR 32	116.5	1 3/8	7/8	18.0		42H1177	42H1176
EVR 32	116.5	1 5/8	7/8	18.0		42H1179	42H1178
EVR 32	116.5	2 1/8	7/8	18.0		42H1181	42H1180
EVR 40	182.0	1 5/8	1	29.0		42H1186	42H1185
EVR 40	182.0	2 1/8	1	29.0		42H1188	

Separate valve bodies for EVR, normally open (NO)

Type	Rated capacity R 22 (liquid) tons	Conne- ction in.	Port size in.	C _v value gal/min	Code nos. valve body excl. coil	
					Flare in.	Solder ODF in.
EVR 6	5.8	3/8	1/4	0.93		32F1164
EVR 10	13.8	1/2	3/8	2.2		32F1169
EVR 15	18.9	5/8	9/16	3.0		32F1174

Coils, see next page

Accessories

Mounting bracket for EVR 2, 3, 4, 6 and 10

Code no. 32F0086

Metric conversions
 1 psi = 0.07 bar
 5/9 (t₁ °F - 32) = t₂ °C
 1 ton = 3.5 kW
 1 in. = 25.4 mm
 US gal/min = 0.86 m³/h

Features


- For high temperatures - class H insulated wire
- Encapsulated coils with long life time
- Wide range of coils
 - from 24 V to 240 V a.c.
 - Junction box and Conduite boss

Approvals

Listed with EVR, MH7648
 Conformity with LVD 73/23/EC with amendments EN 60730-2-8

Note: These approvals are only recognized when one of the EVR series of solenoid valves found in this leaflet is combined with a GP (General purpose) coil

Ordering


Voltage V	Frequency Hz	Code no.		Power consumption
		Junction Box NEMA 2	Conduit Boss NEMA 4	
24	50/60	018F7683	018F7693	Holding: 14 W 28 VA Inrush: 49VA
110	50/60	018F7682	018F7692	
120	60			
208-240	60	018F7681	018F7691	
230	50			

Technical data

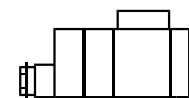
Design	In accordance with UL 429
Power supply	Alternating current (a.c.)
Permissible voltage variation	Alternating current (a.c.): +10 → -15%
Power consumption	Alternating current (a.c.): Inrush: 49 VA; Holding: 28 VA, 14 W
Insulation of coil wire	Class H according to IEC 85
Connection	Junction box or Conduit boss
Enclosure, IEC 529	Junction box NEMA 1 ~ IP 12-32 / Conduit boss NEMA ~ 4 IP 54
Ambient temperature	-40 → 122°F (-40 → +50°C)

Features


- For high temperatures - class H insulated wire
- Encapsulated coils with long life time
- Wide range of coils
 - from 12 V to 200 V d.c.
 - with terminal box IP 67 ~ NEMA 6

Approvals

Conformity with LVD 73/23/EC with amendments EN 60730-2-8

Ordering


Voltage V	Code no.		Power consumption
	For EVR 2-15 EVR 25-40	For EVR 20-22	
12	018F6856	018F6886	Holding: 20 W
12	018F6857	018F6887	
48	018F6859	018F6889	
110	018F6860	018F6890	
115	018F6861	018F6891	
220	018F6851	018F6881	

Technical data

Design	In accordance with VDE 0580
Power supply	Direct current (d.c.)
Permissible voltage variation	+10 → -10%
Power consumption	20 W
Insulation of coil wire	Class H according to IEC 85
Connection	Terminal box
Enclosure, IEC 529	IP67 NEMA ~ 6
Ambient temperature	-40 → 122°F (-40 → +50°C)

Capacity
Note:

Bold figures refer to rated capacity

Liquid

Type	Liquid capacity Q0 tons at a pressure drop across valve Δp psi						
	1	2	3	4	5	6	7

R 22

EVR 2	0.67	0.95	1.17	1.35	1.50	1.65	1.78
EVR 3	1.18	1.66	2.03	2.35	2.63	2.88	3.11
EVR 4	2.40	3.39	4.15	4.79	5.36	5.87	6.34
EVR 6	3.37	4.76	5.83	6.73	7.52	8.24	8.90
EVR 8	4.62	6.54	8.01	9.24	10.3	11.3	12.2
EVR 10	7.99	11.3	13.8	16.0	17.9	19.6	21.1
EVR 15	10.9	15.5	18.9	21.9	24.4	26.8	28.9
EVR 18	14.2	20.1	24.6	28.4	31.8	34.8	37.6
EVR 20	21.0	29.7	36.4	42.0	47.0	51.5	55.6
EVR 22	25.2	35.7	43.7	50.4	56.4	61.8	66.7
EVR 25	42.1	59.5	72.8	84.1	94.0	103.0	111.0
EVR 32	67.3	95.1	116.5	134.0	150.0	164.8	177.0
EVR 40	105.0	148.6	182.0	210.0	235.0	257.0	278.0

R 134a

EVR 2	0.63	0.89	1.09	1.25	1.40	1.54	1.66
EVR 3	1.10	1.55	1.90	2.19	2.45	2.68	2.90
EVR 4	2.23	3.16	3.87	4.47	5.00	5.47	5.91
EVR 6	3.14	4.43	5.43	6.27	7.01	7.68	8.30
EVR 8	4.31	6.09	7.46	8.62	9.63	10.6	11.4
EVR 10	7.45	10.5	12.9	14.9	16.7	18.2	19.7
EVR 15	10.2	14.4	17.7	20.4	22.8	25.0	27.0
EVR 18	13.3	18.7	23.0	26.5	29.6	32.4	35.0
EVR 20	19.6	27.7	33.9	39.2	43.8	48.0	51.8
EVR 22	23.5	33.3	40.7	47.0	52.6	57.6	62.2
EVR 25	39.2	55.4	67.9	78.4	87.6	96.0	103.0
EVR 32	62.7	88.7	108.0	125.0	140.0	153.0	165.0
EVR 40	98.0	138.5	169.0	195.0	219.0	239.0	259.0

R 404A and R 507

EVR	0.46	0.66	0.80	0.93	1.04	1.13	1.23
EVR 3	0.81	1.14	1.40	1.62	1.81	1.98	2.14
EVR 4	1.65	2.33	2.86	3.30	3.69	4.04	4.37
EVR 6	2.32	3.28	4.01	4.63	5.18	5.67	6.13
EVR 8	3.18	4.50	5.52	6.37	7.12	7.80	8.42
EVR 10	5.50	7.78	9.53	11.0	12.3	13.5	14.6
EVR 15	7.53	10.6	13.0	15.1	16.8	18.4	19.9
EVR 18	9.79	13.8	17.0	19.6	21.9	24.0	25.9
EVR 20	14.5	20.5	25.1	29.0	32.4	35.5	38.3
EVR 22	17.4	24.6	30.1	34.7	38.8	42.5	46.0
EVR 25	29.0	40.9	50.2	57.9	64.7	70.9	76.6
EVR 32	46.3	65.5	80.3	92.6	103.6	113.0	121.0
EVR 40	72.4	102.0	125.0	144.0	162.0	177.0	191.0

Capacities are based on
Liquid temperature $t_l = 100^\circ\text{F}$
Evaporating temperature $t_e = 40^\circ\text{F}$
Superheat temperature ($t_e + 10^\circ\text{F}$)
 $= 50^\circ\text{F}$

Metric conversions
1 psi = 0.07 bar
 $5/9 (t_1^\circ\text{F} - 32) = t_2^\circ\text{C}$
1 ton = 3.5 kW

Correction factors for liquid temperature t_l
When liquid temperature t_l ahead of the expansion valve is other than 100°F , adjust the table capacities by multiplying them by the appropriate correction factor found in the following table.

t_l °F	80	90	100	110	120
Factor	1.10	1.05	1.00	0.95	0.90

Capacity (continued)

Suction vapor

R 22

Note:
Bold figures refer to rated capacity

Type	Pressure drop across valve Δp psi	Suction vapor capacity Q_0 tons at evaporating temperature t_e °F							
		- 40	- 20	0	+10	+20	+30	+40	+50
EVR 2	1	0.04	0.05	0.06	0.07	0.08	0.09	0.10	0.11
	2	0.05	0.07	0.09	0.10	0.11	0.12	0.14	0.15
	3	0.06	0.08	0.10	0.12	0.13	0.15	0.17	0.18
EVR 3	1	0.06	0.09	0.11	0.12	0.14	0.15	0.17	0.19
	2	0.09	0.12	0.15	0.18	0.19	0.22	0.24	0.26
	3	0.10	0.14	0.18	0.20	0.23	0.26	0.29	0.32
EVR 4	1	0.13	0.18	0.22	0.25	0.28	0.31	0.34	0.38
	2	0.18	0.24	0.31	0.36	0.40	0.44	0.49	0.54
	3	0.21	0.28	0.37	0.42	0.47	0.54	0.60	0.66
EVR 6	1	0.18	0.25	0.32	0.35	0.39	0.44	0.48	0.53
	2	0.25	0.33	0.43	0.50	0.56	0.62	0.68	0.75
	3	0.29	0.40	0.52	0.59	0.66	0.76	0.84	0.92
EVR 8	1	0.25	0.34	0.43	0.49	0.54	0.60	0.66	0.73
	2	0.34	0.46	0.59	0.69	0.77	0.85	0.94	1.03
	3	0.40	0.55	0.71	0.80	0.91	1.04	1.15	1.26
EVR 10	1	0.44	0.59	0.75	0.84	0.94	1.04	1.15	1.26
	2	0.59	0.79	1.02	1.19	1.32	1.47	1.62	1.78
	3	0.69	0.94	1.23	1.39	1.57	1.80	1.98	2.18
EVR 15	1	0.60	0.81	1.02	1.15	1.28	1.42	1.57	1.72
	2	0.80	1.08	1.40	1.63	1.81	2.01	2.22	2.44
	3	0.94	1.29	1.68	1.90	2.14	2.46	2.71	2.99
EVR 18	1	0.78	1.05	1.33	1.50	1.66	1.84	2.04	2.24
	2	1.04	1.41	1.82	2.12	2.35	2.61	2.88	3.17
	3	1.22	1.68	2.19	2.47	2.79	3.20	3.53	3.88
EVR 20	1	1.15	1.56	1.97	2.22	2.46	2.72	3.02	3.32
	2	1.54	2.08	2.69	3.13	3.48	3.86	4.27	4.69
	3	1.81	2.48	3.23	3.66	4.12	4.73	5.22	5.74
EVR 22	1	1.38	1.87	2.36	2.66	2.95	3.27	3.62	3.98
	2	1.85	2.50	3.23	3.76	4.18	4.63	5.12	5.63
	3	2.17	2.97	3.88	4.39	4.94	5.67	6.26	6.89
EVR 25	1	2.30	3.12	3.94	4.43	4.92	5.45	6.04	6.63
	2	3.09	4.17	5.38	6.27	6.96	7.71	8.53	9.39
	3	3.61	4.96	6.47	7.32	8.24	9.45	10.4	11.5
EVR 32	1	3.68	4.99	6.30	7.09	7.88	8.72	9.66	10.6
	2	4.94	6.67	8.61	10.0	11.1	12.3	13.6	15.0
	3	5.78	7.93	10.4	11.7	13.2	15.1	16.7	18.4
EVR 40	1	5.74	7.80	9.85	11.1	12.3	13.6	16.1	16.6
	2	7.71	10.4	13.5	15.7	17.4	19.3	21.3	23.5
	3	9.03	12.4	16.2	18.3	20.6	23.6	26.1	28.7

The table values refer to evaporator capacity and are given as a function of evaporating temperature t_e and pressure drop Δp across the valve.

Capacities are based on liquid temperature $t_l = 100^\circ\text{F}$ ahead of the expansion valve and superheat $t_s = 7^\circ\text{F}$.

For each additional 10°F of superheat, the table capacities must be reduced by 2%.

Correction factors for liquid temperature t_l
When liquid temperature t_l ahead of the expansion valve is other than 100°F , adjust the table capacities by multiplying them by the appropriate correction factor found in the following table.

t_l °F	80	90	100	110	120
Factor	1.10	1.05	1.00	0.95	0.90

Metric conversions
1 psi = 0.07 bar
 $5/9 (t_1^\circ\text{F} - 32) = t_2^\circ\text{C}$
1 ton = 3.5 kW

Capacity (continued)

Note:
Bold figures refer to rated capacity

Suction vapor
R 134a

Type	Pressure drop across valve Δp psi	Suction vapor capacity Q_0 tons at evaporating temperature t_e °F							
		- 40	- 20	0	+10	+20	+30	+40	+50
EVR 2	1	0.02	0.03	0.05	0.05	0.06	0.07	0.07	0.08
	2	0.03	0.04	0.06	0.07	0.08	0.09	0.11	0.12
	3	0.03	0.05	0.07	0.08	0.10	0.11	0.12	0.14
EVR 3	1	0.04	0.06	0.08	0.09	0.10	0.12	0.13	0.14
	2	0.05	0.08	0.10	0.12	0.14	0.16	0.18	0.21
	3	0.06	0.09	0.12	0.14	0.17	0.19	0.22	0.25
EVR 4	1	0.08	0.11	0.16	0.18	0.21	0.24	0.26	0.30
	2	0.10	0.15	0.21	0.25	0.28	0.33	0.37	0.42
	3	0.11	0.18	0.25	0.30	0.34	0.39	0.44	0.51
EVR 6	1	0.11	0.16	0.23	0.26	0.29	0.33	0.37	0.42
	2	0.14	0.22	0.30	0.35	0.40	0.47	0.53	0.59
	3	0.16	0.25	0.35	0.42	0.48	0.55	0.62	0.72
EVR 8	1	0.16	0.22	0.31	0.35	0.40	0.45	0.51	0.57
	2	0.20	0.30	0.41	0.48	0.55	0.64	0.72	0.81
	3	0.22	0.34	0.49	0.57	0.65	0.75	0.85	0.99
EVR 10	1	0.27	0.38	0.54	0.61	0.69	0.79	0.88	0.99
	2	0.34	0.51	0.71	0.82	0.94	1.11	1.25	1.40
	3	0.37	0.59	0.84	0.99	1.13	1.30	1.47	1.71
EVR 15	1	0.37	0.52	0.73	0.84	0.95	1.08	1.20	1.35
	2	0.47	0.70	0.97	1.13	1.29	1.52	1.71	1.91
	3	0.51	0.80	1.15	1.35	1.54	1.78	2.01	2.34
EVR 18	1	0.48	0.68	0.95	1.09	1.23	1.40	1.56	1.75
	2	0.61	0.91	1.26	1.46	1.68	1.98	2.22	2.49
	3	0.67	1.04	1.50	1.75	2.01	2.31	2.62	3.04
EVR 20	1	0.71	1.00	1.41	1.61	1.82	2.07	2.31	2.59
	2	0.90	1.35	1.87	2.17	2.48	2.92	3.28	3.68
	3	0.98	1.54	2.22	2.59	2.97	3.41	3.87	4.50
EVR 22	1	0.85	1.20	1.69	1.93	2.19	2.48	2.78	3.11
	2	1.08	1.62	2.25	2.60	2.97	3.51	3.94	4.41
	3	1.18	1.85	2.66	3.11	3.56	4.10	4.65	5.40
EVR 25	1	1.41	2.00	2.82	3.22	3.64	4.14	4.63	5.19
	2	1.81	2.69	3.74	4.33	4.96	5.84	6.56	7.35
	3	1.97	3.09	4.43	5.19	5.94	6.83	7.75	8.99
EVR 32	1	2.26	3.20	4.52	5.15	5.83	6.62	7.40	8.30
	2	2.89	4.31	5.99	6.93	7.93	9.35	10.5	11.8
	3	3.15	4.94	7.09	8.30	9.51	10.9	12.4	14.4
EVR 40	1	3.53	5.01	7.06	8.04	9.11	10.3	11.6	13.0
	2	4.51	6.73	9.35	10.8	12.4	14.6	16.4	18.4
	3	4.92	7.71	11.1	13.0	14.9	17.1	19.4	22.5

The table values refer to evaporator capacity and are given as a function of evaporating temperature t_e and pressure drop Δp across the valve.

Capacities are based on liquid temperature $t_l = 100^\circ\text{F}$ ahead of the expansion valve and superheat $t_s = 7^\circ\text{F}$.

For each additional 10°F of superheat, the table capacities must be reduced by 2%.

Correction factors for liquid temperature t_l

When liquid temperature t_l ahead of the expansion valve is other than 100°F , adjust the table capacities by multiplying them by the appropriate correction factor found in the following table.

t_l °F	80	90	100	110	120
Factor	1.10	1.05	1.00	0.95	0.90

Metric conversions

1 psi = 0.07 bar

5/9 ($t_1^\circ\text{F} - 32$) = $t_2^\circ\text{C}$

1 ton = 3.5 kW

Capacity (continued)

Suction vapor

R 404A and R 507

Note:
Bold figures refer to rated capacity

Type	Pressure drop across valve Δp psi	Suction vapor capacity Q_0 tons at evaporating temperature t_e °F							
		- 40	- 20	0	+10	+20	+30	+40	+50
EVR 2	1	0.03	0.04	0.05	0.06	0.07	0.08	0.09	0.10
	2	0.04	0.05	0.08	0.09	0.10	0.11	0.12	0.13
	3	0.05	0.06	0.09	0.10	0.12	0.13	0.15	0.16
EVR 3	1	0.05	0.07	0.09	0.11	0.12	0.13	0.15	0.17
	2	0.07	0.09	0.13	0.15	0.17	0.19	0.21	0.23
	3	0.08	0.11	0.15	0.18	0.20	0.23	0.26	0.29
EVR 4	1	0.10	0.14	0.19	0.22	0.24	0.27	0.30	0.34
	2	0.14	0.19	0.27	0.30	0.34	0.39	0.43	0.48
	3	0.16	0.23	0.31	0.36	0.42	0.47	0.53	0.59
EVR 6	1	0.14	0.20	0.26	0.30	0.34	0.38	0.43	0.48
	2	0.20	0.27	0.38	0.43	0.48	0.54	0.60	0.67
	3	0.23	0.32	0.44	0.50	0.59	0.66	0.74	0.82
EVR 8	1	0.20	0.27	0.36	0.42	0.47	0.52	0.58	0.65
	2	0.27	0.37	0.52	0.58	0.66	0.74	0.83	0.92
	3	0.32	0.44	0.60	0.69	0.80	0.91	1.01	1.13
EVR 10	1	0.34	0.47	0.62	0.72	0.80	0.90	1.01	1.13
	2	0.47	0.64	0.89	1.01	1.14	1.28	1.43	1.60
	3	0.55	0.77	1.04	1.20	1.39	1.57	1.75	1.96
EVR 15	1	0.47	0.65	0.85	0.99	1.10	1.24	1.38	1.54
	2	0.64	0.88	1.22	1.38	1.55	1.76	1.95	2.18
	3	0.75	1.05	1.43	1.64	1.90	2.15	2.40	2.68
EVR 18	1	0.61	0.84	1.11	1.29	1.43	1.61	1.80	2.01
	2	0.83	1.14	1.59	1.80	2.02	2.29	2.54	2.84
	3	0.98	1.36	1.85	2.13	2.47	2.80	3.12	3.48
EVR 20	1	0.90	1.25	1.64	1.90	2.12	2.38	2.66	2.97
	2	1.23	1.69	2.35	2.66	2.99	3.38	3.76	4.20
	3	1.44	2.02	2.74	3.15	3.66	4.14	4.61	5.15
EVR 22	1	1.08	1.50	1.97	2.28	2.54	2.86	3.19	3.56
	2	1.48	2.03	2.82	3.19	3.58	4.06	4.51	5.04
	3	1.73	2.42	3.29	3.78	4.39	4.96	5.53	6.18
EVR 25	1	1.81	2.49	3.28	3.81	4.23	4.76	5.32	5.94
	2	2.46	3.38	4.69	5.32	5.97	6.76	7.52	8.40
	3	2.89	4.04	5.48	6.30	7.32	8.27	9.22	10.31
EVR 32	1	2.89	3.99	5.25	6.09	6.77	7.62	8.51	9.51
	2	3.94	5.41	7.51	8.51	9.56	10.8	12.0	13.4
	3	4.62	6.46	8.77	10.1	11.7	13.2	14.8	16.5
EVR 40	1	4.51	6.24	8.21	9.5	10.6	11.9	13.3	14.9
	2	6.15	8.45	11.7	13.3	14.9	16.9	18.8	21.0
	3	7.22	10.1	13.7	15.8	18.3	20.7	23.1	25.8

The table values refer to evaporator capacity and are given as a function of evaporating temperature t_e and pressure drop Δp across the valve.

Capacities are based on liquid temperature $t_l = 100^\circ\text{F}$ ahead of the expansion valve and superheat $t_s = 7^\circ\text{F}$.

For each additional 10°F of superheat, the table capacities must be reduced by 2%.

Correction factors for liquid temperature t_l

When liquid temperature t_l ahead of the expansion valve is other than 100°F , adjust the table capacities by multiplying them by the appropriate correction factor found in the following table.

t_l °F	80	90	100	110	120
Factor	1.10	1.05	1.00	0.90	0.90

Metric conversions

1 psi = 0.07 bar

5/9 ($t_1^\circ\text{F} - 32$) = $t_2^\circ\text{C}$

1 ton = 3.5 kW

Capacity (continued)

Hot gas

EVR 2 to EVR 18

Note:
Bold figures refer to rated capacity

Type	Pressure drop across valve Δp psi	Hot gas capacity Q_h tons								
		Evaporating temp. $t_e = +40^\circ\text{F}$, hot gas temp. $t_h = t_c + 40^\circ\text{F}$, subcooling $\Delta t_{sl} = 10^\circ\text{F}$								
		R 22			R 134a			R 404A/R 507		
		Condensing temp. t_c °F			Condensing temp. t_c °F			Condensing temp. t_c °F		
	+70	+100	+140	+70	+100	+140	+70	+100	+140	
EVR 2	2	0.20	0.22	0.23	0.16	0.18	0.18	0.17	0.17	0.17
	5	0.31	0.35	0.37	0.26	0.28	0.29	0.27	0.28	0.27
	10	0.43	0.49	0.53	0.35	0.39	0.42	0.37	0.40	0.38
	15	0.53	0.58	0.65	0.43	0.48	0.52	0.45	0.47	0.47
	20	0.60	0.67	0.73	0.50	0.56	0.59	0.52	0.54	0.53
	25	0.67	0.75	0.81	0.56	0.63	0.66	0.58	0.61	0.59
EVR 3	2	0.34	0.38	0.41	0.28	0.31	0.32	0.29	0.30	0.29
	5	0.55	0.60	0.64	0.45	0.49	0.51	0.47	0.48	0.47
	10	0.75	0.86	0.92	0.62	0.69	0.74	0.64	0.70	0.67
	15	0.92	1.02	1.14	0.76	0.84	0.91	0.79	0.82	0.82
	20	1.05	1.18	1.27	0.88	0.97	1.03	0.90	0.94	0.92
	25	1.18	1.31	1.42	0.99	1.09	1.15	1.02	1.06	1.03
EVR 4	2	0.70	0.77	0.83	0.57	0.63	0.66	0.59	0.62	0.60
	5	1.12	1.23	1.32	0.92	1.01	1.05	0.95	0.99	0.95
	10	1.54	1.76	1.88	1.26	1.40	1.50	1.30	1.42	1.36
	15	1.87	2.08	2.32	1.54	1.72	1.87	1.60	1.67	1.68
	20	2.15	2.40	2.59	1.79	1.99	2.10	1.85	1.93	1.88
	25	2.40	2.67	2.89	2.01	2.23	2.35	2.07	2.17	2.09
EVR 6	2	0.98	1.08	1.16	0.80	0.88	0.92	0.83	0.87	0.84
	5	1.57	1.73	1.85	1.29	1.41	1.47	1.33	1.39	1.34
	10	2.16	2.47	2.63	1.77	1.96	2.11	1.83	1.99	1.91
	15	2.63	2.92	3.26	2.17	2.41	2.62	2.25	2.35	2.36
	20	3.02	3.37	3.64	2.51	2.79	2.94	2.59	2.70	2.63
	25	3.37	3.75	4.06	2.82	3.13	3.30	2.91	3.04	2.94
EVR 8	2	1.35	1.49	1.60	1.10	1.21	1.27	1.14	1.19	1.16
	5	2.15	2.37	2.54	1.78	1.94	2.03	1.83	1.91	1.84
	10	2.97	3.40	3.62	2.43	2.70	2.90	2.52	2.74	2.62
	15	3.61	4.01	4.48	2.98	3.31	3.60	3.09	3.23	3.25
	20	4.15	4.62	5.00	3.45	3.83	4.05	3.56	3.71	3.62
	25	4.63	5.16	5.58	3.88	4.30	4.54	4.00	4.18	4.04
EVR 10	2	2.33	2.57	2.76	1.90	2.10	2.20	1.98	2.06	2.00
	5	3.72	4.10	4.38	3.07	3.36	3.50	3.16	3.29	3.17
	10	5.13	5.87	6.26	4.20	4.66	5.01	4.35	4.73	4.53
	15	6.24	6.93	7.74	5.15	5.72	6.22	5.34	5.58	5.61
	20	7.17	7.99	8.63	5.96	6.62	6.99	6.15	6.42	6.26
	25	8.00	8.91	9.64	6.70	7.43	7.85	6.90	7.22	6.98
EVR 15	2	3.18	3.52	3.77	2.60	2.87	3.00	2.71	2.82	2.73
	5	5.09	5.61	6.00	4.20	4.59	4.79	4.33	4.51	4.34
	10	7.02	8.04	8.56	5.74	6.38	6.85	5.95	6.47	6.20
	15	8.54	9.48	10.6	7.04	7.83	8.51	7.31	7.63	7.67
	20	9.81	10.9	11.8	8.16	9.06	9.57	8.41	8.78	8.56
	25	10.9	12.2	13.2	9.2	10.2	10.7	9.45	9.88	9.55
EVR 18	2	4.14	4.57	4.90	3.38	3.73	3.91	3.52	3.67	3.55
	5	6.62	7.29	7.80	5.46	5.97	6.22	5.63	5.86	5.65
	10	9.13	10.5	11.1	7.47	8.29	8.91	7.73	8.41	8.07
	15	11.1	12.3	13.8	9.15	10.2	11.1	9.51	9.92	9.98
	20	12.8	14.2	15.4	10.6	11.8	12.4	10.9	11.4	11.1
	25	14.2	15.9	17.2	11.9	13.2	14.0	12.3	12.9	12.4

Correction factors for t_h and t_e

The table values refer to hot gas capacity and are given as a function of condensing temperature t_c and pressure drop Δp across the valve.

Capacities are based on a hot gas temperature superheated 40°F above condensing temperature ($t_h = t_c + 40^\circ\text{F}$).

For each additional 10°F of superheat above 40°F , the table capacities must be reduced by 1%.

When the valve is used in a hot gas defrost circuit, evaporator temperature affects the capacity.

When the evaporator temperature differs from $+40^\circ\text{F}$, adjust the table capacities by multiplying them by the appropriate correction factor found in the following table.

t_e °F	-40	-20	0	20	40	50
Factor	1.18	1.14	1.09	1.04	1	0.97

Metric conversions

1 psi = 0.07 bar

$5/9 (t_1 - 32) = t_2$ °C

1 ton = 3.5 kW

Capacity (continued)

Hot gas

EVR 20 to EVR 40

Note:
Bold figures refer to rated capacity

Type	Pressure drop across valve Δp psi	Hot gas capacity Q_h tons								
		Evaporating temp. $t_e = +40^\circ\text{F}$, hot gas temp. $t_h = t_c + 40^\circ\text{F}$, subcooling $\Delta t_u = 10^\circ\text{F}$								
		R 22			R 134a			R 404A/R 507		
		Condensing temp. t_c °F			Condensing temp. t_c °F			Condensing temp. t_c °F		
		+70	+100	+140	+70	+100	+140	+70	+100	+140
EVR 20	2	6.12	6.76	7.25	5.01	5.51	5.78	5.20	5.43	5.25
	5	9.80	10.8	11.5	8.07	8.83	9.21	8.32	8.67	8.35
	10	13.5	15.5	16.5	11.1	12.3	13.2	11.4	12.4	11.9
	15	16.4	18.2	20.4	13.5	15.1	16.4	14.1	14.7	14.8
	20	18.9	21.0	22.7	15.7	17.4	18.4	16.2	16.9	16.5
	25	21.0	23.5	25.4	17.6	19.6	20.7	18.2	19.0	18.4
EVR 22	2	7.35	8.11	8.71	6.01	6.62	6.93	6.24	6.52	6.30
	5	11.8	12.9	13.9	9.69	10.6	11.1	9.99	10.4	10.0
	10	16.2	18.6	19.8	13.3	14.7	15.8	13.7	14.9	14.3
	15	19.7	21.9	24.4	16.3	18.1	19.6	16.9	17.6	17.7
	20	22.7	25.2	27.3	18.8	20.9	22.1	19.4	20.3	19.8
	25	25.3	28.1	30.5	21.2	23.5	24.8	21.8	22.8	22.0
EVR 25	2	12.2	13.5	14.5	10.0	11.0	11.6	10.4	10.9	10.5
	5	19.6	21.6	23.1	16.2	17.7	18.4	16.6	17.3	16.7
	10	27.0	30.9	32.9	22.1	24.5	26.4	22.9	24.9	23.9
	15	32.9	36.5	40.7	27.1	30.1	32.7	28.1	29.4	29.5
	20	37.8	42.1	45.4	31.4	34.9	36.8	32.4	33.8	32.9
	25	42.1	46.9	50.8	35.3	39.1	41.3	36.3	38.0	36.7
EVR 32	2	19.6	21.6	23.2	16.0	17.7	18.5	16.7	17.4	16.8
	5	31.4	34.5	36.9	25.8	28.3	29.5	26.6	27.7	26.7
	10	43.2	49.5	52.7	35.3	39.2	42.2	36.6	39.8	28.2
	15	52.6	58.4	65.2	43.3	48.2	52.4	45.0	47.0	47.2
	20	60.4	67.3	72.7	50.2	55.8	58.9	51.8	54.0	52.7
	25	67.3	75.1	81.2	56.4	62.6	66.1	58.1	60.3	58.8
EVR 40	2	30.6	33.8	36.3	25.0	27.6	28.9	26.0	27.2	26.3
	5	49.0	53.9	57.7	40.4	44.2	46.0	41.6	43.3	41.8
	10	67.5	77.3	82.3	55.2	61.3	65.9	57.2	62.2	59.7
	15	82.1	91.1	101.0	67.7	75.3	81.8	70.3	73.4	73.8
	20	94.4	105.0	113.0	78.5	87.2	92.0	80.9	84.4	82.3
	25	105.0	117.0	126.0	88.1	97.8	103.0	90.8	95.0	91.8

Correction factors for t_h and t_e

The table values refer to hot gas capacity and are given as a function of condensing temperature t_c and pressure drop Δp across the valve.

Capacities are based on a hot gas temperature superheated 40°F above condensing temperature ($t_h = t_c + 40^\circ\text{F}$).

For each additional 10°F of superheat above 40°F , the table capacities must be reduced by 1%.

When the valve is used in a hot gas defrost circuit, evaporator temperature affects the capacity.

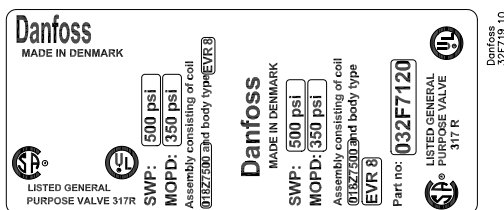
When the evaporator temperature differs from $+40^\circ\text{F}$, adjust the table capacities by multiplying them by the appropriate correction factor found in the following table.

t_e °F	-40	-20	0	20	40	50
Factor	1.18	1.14	1.09	1.04	1	0.97

Metric conversions

1 psi = 0.07 bar
 $5/9 (t_1^\circ\text{F} - 32) = t_2^\circ\text{C}$
 1 ton = 3.5 kW

Identification



Essential valve data is given on the label

Example

- EVR 8 = Valve type and size
- HFC-HCFC = Fluorinated refrigerants
- SWP = Safe Working Pressure (MWP) in psig
- 018Z7600 = Coil group for the EVR
- MOPD = Maximum Operating Pressure in psi
- S and A = Approvals in USA and Canada

Valve selection example

Note: When selecting the appropriate solenoid valve, it is easier to convert the actual required capacity to that of the rated capacities listed in the tables. This is done by utilizing various correction factors in the selection process. The following examples illustrate how this is done.

Liquid line solenoid valve selection example

Refrigerant = R134a
 Condensing temperature $t_c = 100^\circ\text{F}$
 Liquid temperature ahead of valve $t_l = 90^\circ\text{F}$
 Maximum allowable pressure drop across valve $\Delta p = 2$ psi
 Evaporator capacity $Q_o = 10$ tons (required valve capacity)

Step 1:

Determine the correction factor for liquid temperature. From the correction factor table found on page 7, a liquid temperature of 90°F corresponds to a factor of 1.05.

Step 2:

Correct the required valve capacity. This is done by dividing the evaporator capacity by the liquid correction factor.
 $Q_{\text{corrected}} = 10 / 1.05 = 9.5$ tons

Step 3:

Select the appropriate capacity table and choose the first valve whose capacity is greater than or equal to $Q_{\text{corrected}}$ at the required pressure drop. Using the R 134a liquid capacity table found on page 7, the EVR 10 is selected as it has a capacity of 10.5 tons at a $\Delta p = 2$ psi.

Suction line solenoid valve selection example

Refrigerant = R134a
 Liquid temperature ahead of expansion valve $t_l = 90^\circ\text{F}$

Evaporator temperature $t_e = 30^\circ\text{F}$
 Superheat ahead of valve $t_s = 17^\circ\text{F}$
 Maximum allowable pressure drop across valve $\Delta p = 3$ psi
 Evaporator capacity $Q_o = 10$ tons (required valve capacity)

Step 1:

Determine the correction factor for superheat ahead of the valve by increasing the required valve capacity by 2% for each 10°F of actual superheat above the table rated value of 7°F . In the example, a superheat of 17°F corresponds to a 10°F increase above the table value which is equivalent to a superheat correction factor of 1.02.

Step 2:

Determine the correction factor for liquid temperature. From the correction factor table found on page 9, a liquid temperature of 90°F corresponds to a factor of 1.05.

Step 3:

Correct the required valve capacity. This is done by first multiplying the evaporator capacity by the superheat correction factor and then dividing it by the liquid correction factor.
 $Q_{\text{corrected}} = (10 \times 1.02) / 1.05 = 9.7$ tons

Step 4:

Select the appropriate capacity table and choose the first valve whose capacity is greater than or equal to $Q_{\text{corrected}}$ at the required evaporating temperature and pressure drop. Using the R 134a suction vapor capacity table found on page 9, the EVR 32 is selected as it has a capacity of 10.9 tons at $t_e = 30^\circ\text{F}$ and $\Delta p = 3$ psi.

Metric conversions

- 1 psi = 0.07 bar
- $5/9 (t_1^\circ\text{F} - 32) = t_2^\circ\text{C}$
- 1 ton = 3.5 kW

Valve selection example

(continued)

Hot gas line solenoid valve selection example

With hot gas defrost, pressure in the evaporator quickly rises to a value near that of the condensing pressure and remains there until the defrost cycle has been completed. Therefore, when selecting valves for hot gas applications, sizing is based primarily on the condensing temperature t_c and the pressure drop Δp across the valve.

Example (with heat recovery)

Refrigerant = R134a

 Evaporator temperature $t_e = 0^\circ\text{F}$

 Condensing temperature $t_c = 100^\circ\text{F}$

 Hot gas temperature ahead of valve $t_h = 180^\circ\text{F}$

Maximum allowable pressure drop across valve

 $\Delta p = 5 \text{ psi}$

 Output of heat recovery condenser $Q_h = 15 \text{ tons}$
 (required valve capacity)

Step 1:

Determine the correction factor for hot gas temperature ($t_h = t_c + 40^\circ\text{F}$) by increasing the required valve capacity by 1% for each 10°F of actual superheat above the table rated superheat value of 40°F .

In the example, an actual hot gas temperature of 180°F is 40°F higher than the calculated table value of ($t_h = t_c + 40^\circ\text{F} = 140^\circ\text{F}$). This is equivalent to a hot gas correction factor of 1.04 (4% higher).

Step 2:

Determine the correction factor for evaporator temperature. From the correction factor table found on page 11, an evaporator temperature of 0°F corresponds to a factor of 1.09.

Step 3:

Correct the required valve capacity. This is done by first multiplying the heat recovery capacity by the hot gas correction factor and then dividing it by the evaporator correction factor.

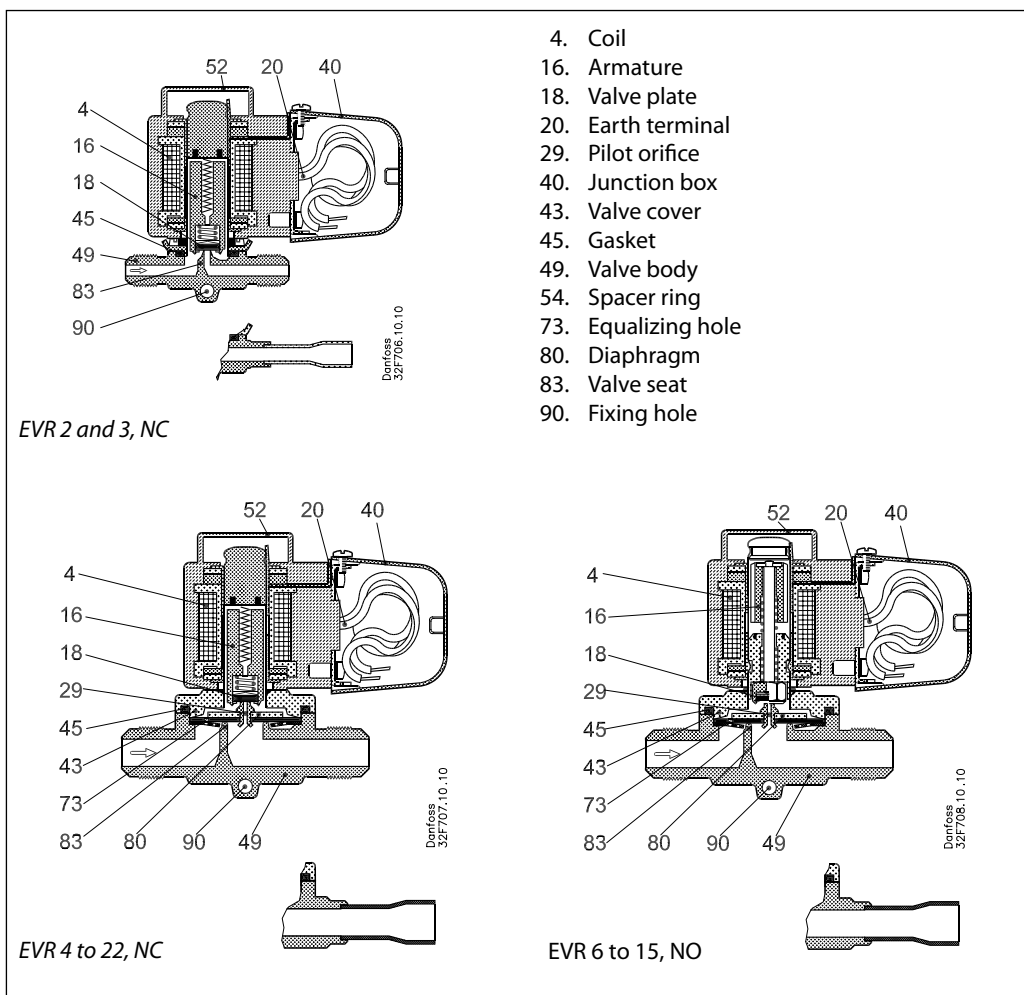
$$Q_{\text{corrected}} = (15 \times 1.04) / 1.09 = 14.3 \text{ tons}$$

Step 4:

Select the appropriate capacity table and choose the first valve whose capacity is greater than or equal to $Q_{\text{corrected}}$ at the required condensing temperature and pressure drop. Using the R 134a hot gas capacity table found on pages 11 and 12, the EVR 25 is selected as it has a capacity of 17.7 tons at $t_c = 100^\circ\text{F}$ and $\Delta p = 5 \text{ psi}$.

Metric conversions
 $1 \text{ psi} = 0.07 \text{ bar}$
 $5/9 (t_1^\circ\text{F} - 32) = t_2^\circ\text{C}$
 $1 \text{ ton} = 3.5 \text{ kW}$

Design



Function

EVR solenoid valves are based on two different design principles:

1. Direct operation
2. Servo operation

1: Direct operation

EVR 2 and 3 are direct-operated. The valve opens to admit full flow when the armature (16) is moved up into the magnetic field of the coil.

The valve operates with a minimum differential pressure of 0 psi.

The valve plate (18) is made of teflon and is fitted directly to the armature (16).

Inlet pressure, spring force and armature weight act to close the valve when the coil is de-energized.

2a: EVR 4 to 22 are servo-operated with a "floating" diaphragm (80). The pilot orifice (29) is located in the center of the diaphragm.

The teflon pilot valve plate (18) is fitted directly to the armature (16).

When the coil is de-energized, the valve port and pilot orifice are closed and the inlet pressure acts both above and below the diaphragm.

The valve port and pilot orifice are kept closed by the weight of the armature, armature spring force and the differential pressure between inlet and outlet sides.

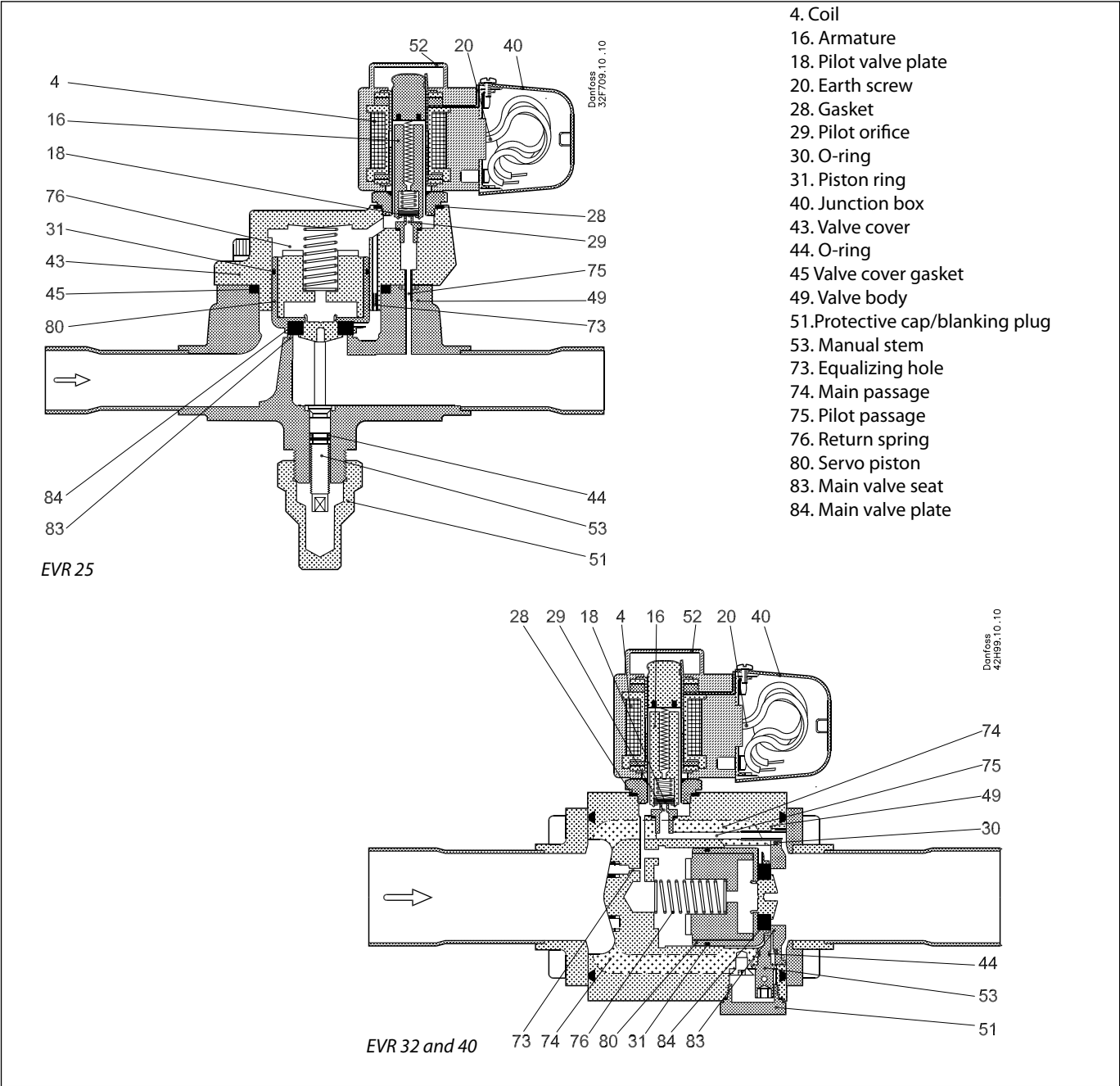
When current is applied to the coil, the armature is pulled up into the magnetic field and the pilot orifice opens. This relieves pressure above the diaphragm because the space above it becomes connected to the outlet side of the valve. The differential pressure between inlet and outlet presses the diaphragm away from the valve seat (83) and the valve opens to admit full flow. A minimum differential pressure (0.7 psi for EVR 4 to 22) is necessary to open the valve and keep it open.

When the coil is de-energized, the pilot orifice closes. Then, via the equalizing port (73) the pressure above the diaphragm rises to the same value as the inlet pressure, which results in the valve port being closed by the diaphragm.

EVR 6 to 15, NO, function in a manner opposite to the NC valves; they are open when the coil is de-energized.

Normally open (NO) EVR valves are available with servo operation only.

Design

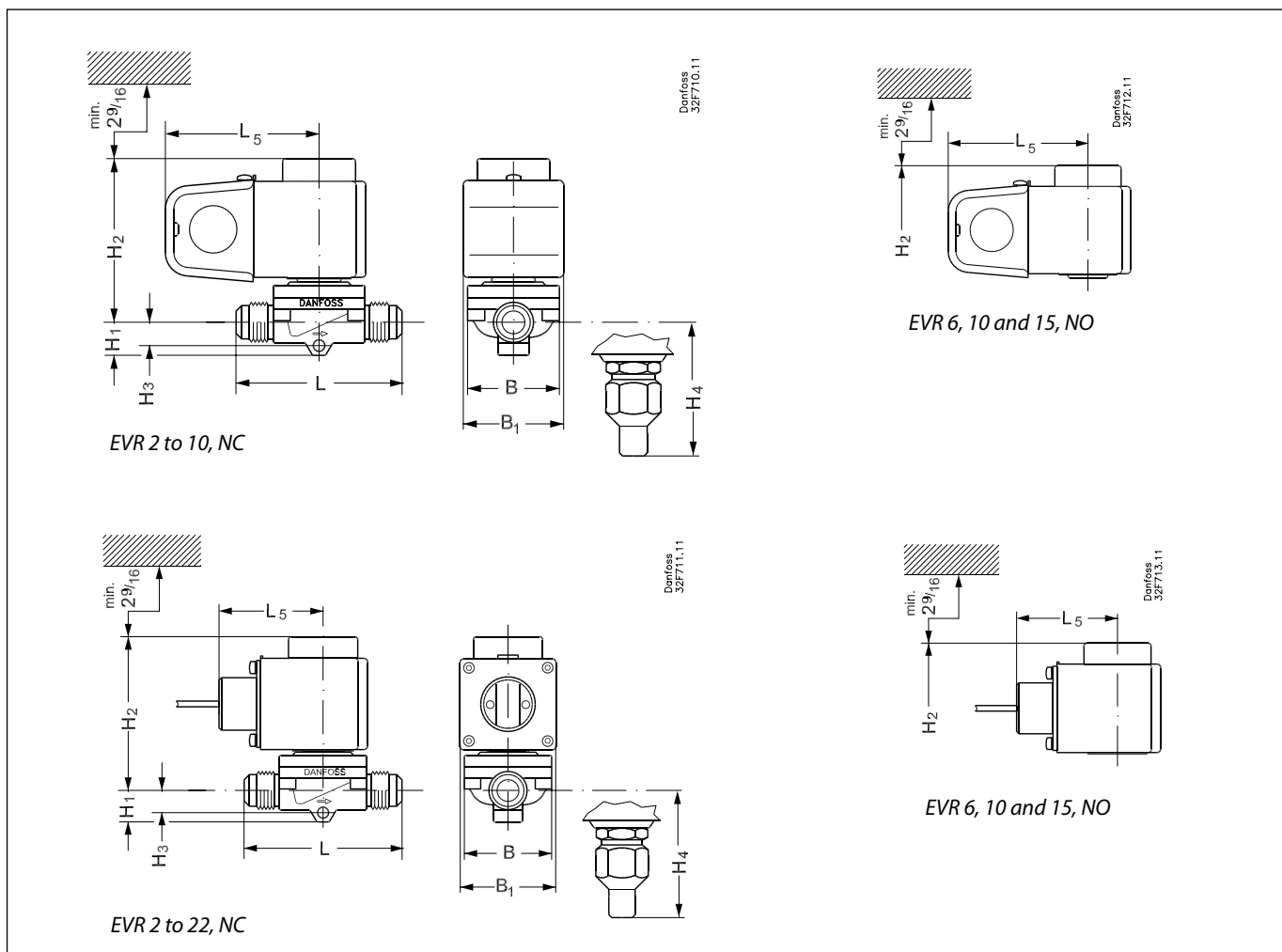


Function

2b. Servo operation of EVR 25 to 40
 EVR 25, 32 and 40 are servo-operated piston valves.
 The valves are closed when the coil is de-energized. In operation, EVR 25 is the same as for EVR 4 to 22, but the design is different. The pilot unit is located in the cover and the servo unit is a piston (80) with a cast iron piston ring.

For EVR 25 to 40, piston (80) and valve plate (84) will close against the valve seat (83) due to the differential pressure between inlet and outlet plus the force from the return spring (76) and the weight of the piston.
 When the coil is energized, the pilot orifice (29) is opened and pressure on the spring side of the piston is relieved. The pressure differential now opens the valve. The minimum differential required to keep the valve fully open is 1 psi.

Dimensions and weights



Flare connection

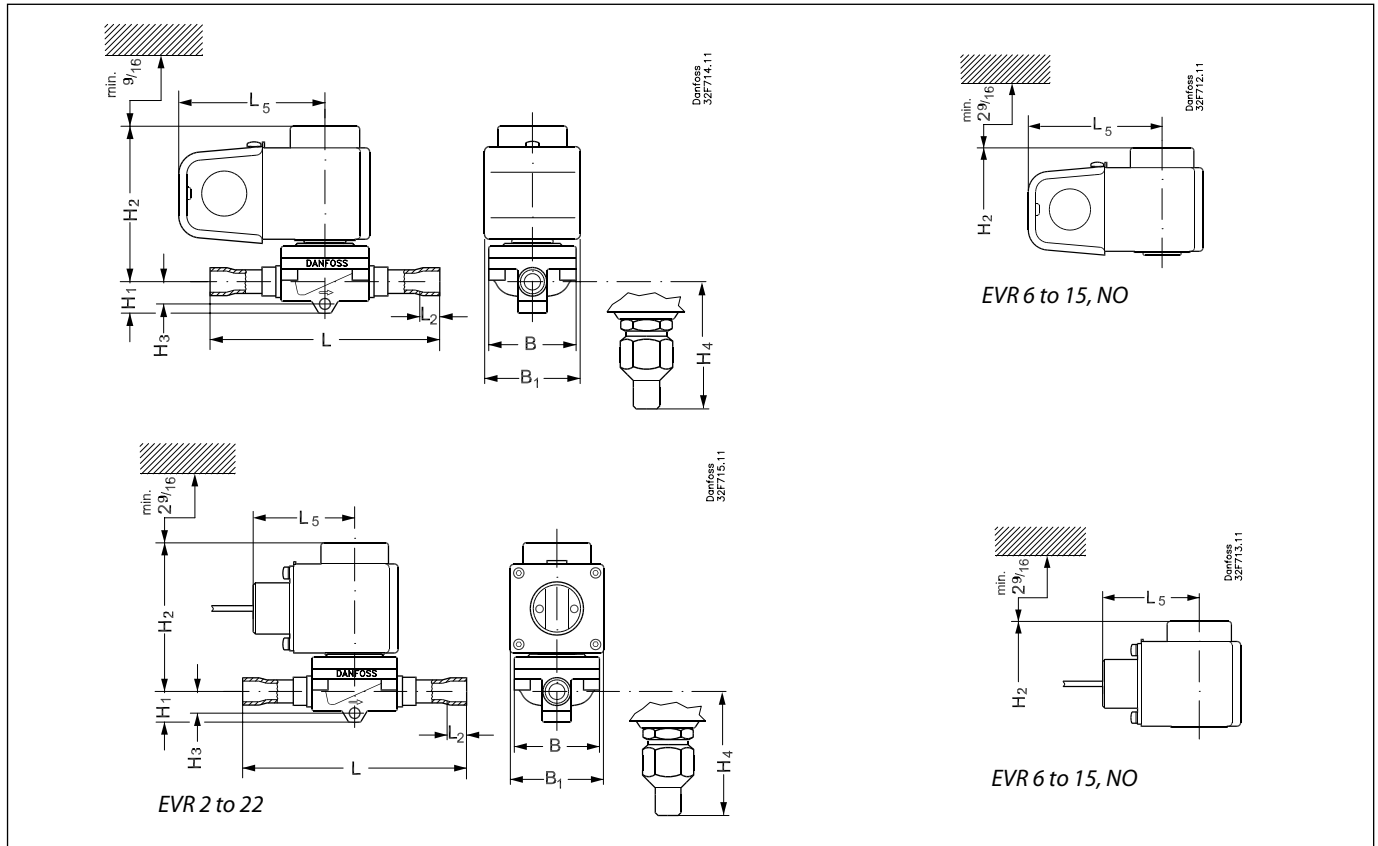
Type	Connection		L in.	L ₅ in.	H ₁ in.	H ₂ NC in.	H ₃ in.	H ₄ in.	B in.	B ₁ in.	Weight with coil lbs
	normal size in.	oversize in.									
	EVR 2, NC	1/4									
EVR 3, NC	1/4		2 5/16	2 3/4	9/16	2 13/16	5/16		1 5/16	2 1/16	1.3
EVR 3, NC		3/8	2 7/16	2 3/4	9/16	2 13/16	5/16		1 5/16	2 1/16	1.3
EVR 4, NC	3/8		2 3/4	2 3/4	9/16	2 7/8	3/8		1 7/16	2 1/16	1.4
EVR 4, NC		1/2	3	2 3/4	9/16	2 7/8	3/8		1 7/16	2 1/16	1.4
EVR 6, NC	3/8		2 3/4	2 3/4	9/16	2 7/8	3/8		1 7/16	2 1/16	1.4
EVR 6, NC	3/8		2 3/4	2 3/4	9/16	2 7/8		2 3/16	1 7/16	2 1/16	1.4
EVR 6, NC		1/2	3	2 3/4	9/16	2 7/8	3/8		1 7/16	2 1/16	1.4
EVR 8, NC	1/2		3 5/16	2 3/4	9/16	2 7/8	3/8		1 7/16	2 1/16	1.4
EVR 10, NC	1/2		3 5/16	2 3/4	9/16	3 1/8	7/16		1 13/16	2 1/16	1.8
EVR 10, NC	1/2		3 5/16	2 3/4	9/16	3 1/8		2 3/16	1 13/16	2 1/16	1.8
EVR 10, NC		5/8	3 5/8	2 3/4	9/16	3 1/8	7/16		1 13/16	2 1/16	1.8

Coil weight: 1lb

Metric conversions

1 in. = 25.4 mm

Dimensions and weights



Solder connection

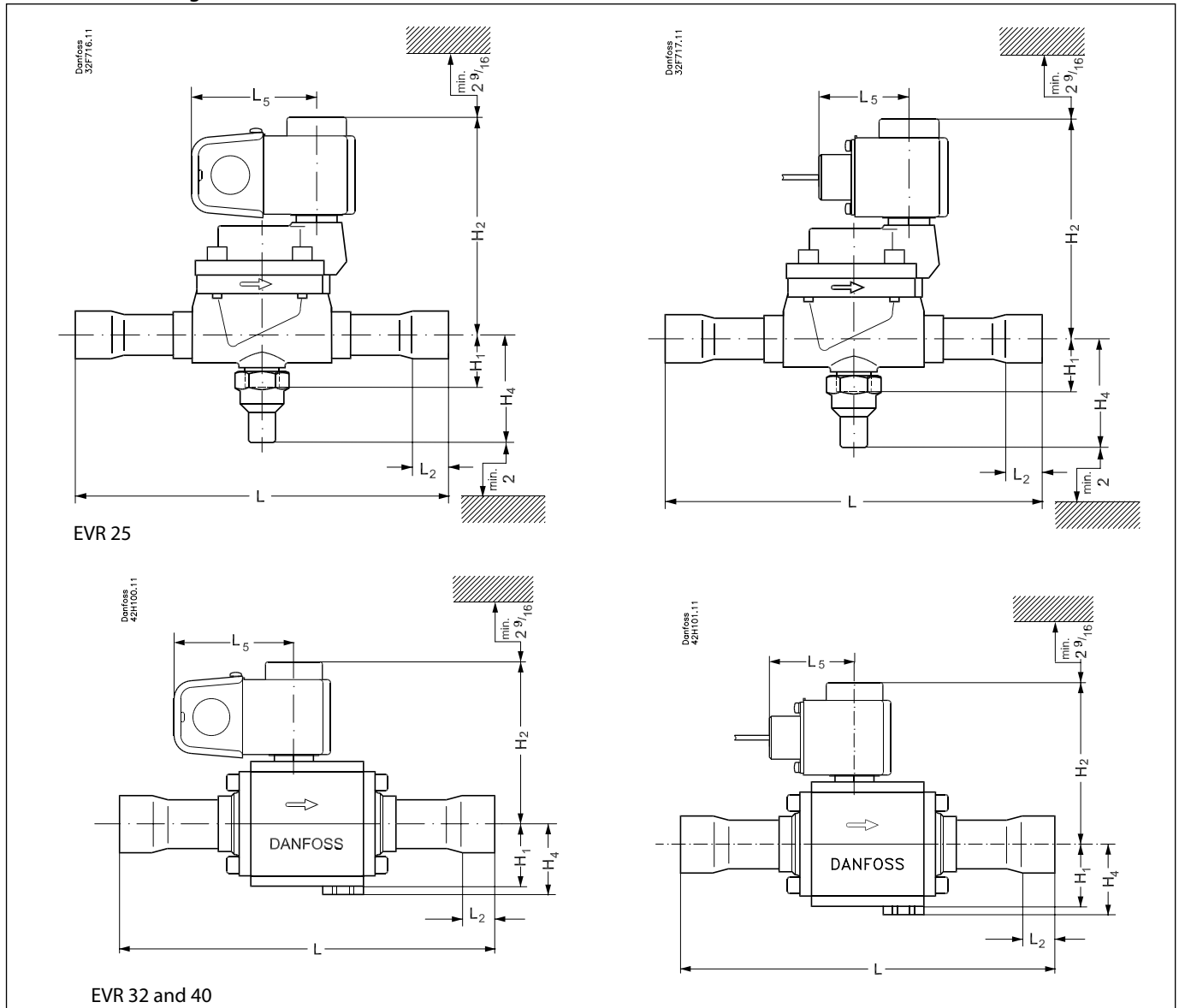
Type	Connection		L in.	L ₂ in.	L ₅ in.	H ₁ in.	H ₂ NC in.	H ₃ in.	H ₄ in.	B in.	B ₁ in.	Weight with coil lbs
	normal size in.	oversize in.										
EVR 2 NC	1/4		4 5/8	3/8	2 3/4	9/16	2 13/16	5/16		1 5/16	2 1/16	1.3
EVR 3 NC	1/4		4 5/8	3/8	2 3/4	9/16	2 13/16	5/16		1 5/16	2 1/16	1.3
EVR 3 NC		3/8	4 5/8	3/8	2 3/4	9/16	2 13/16	5/16		1 5/16	2 1/16	1.3
EVR 4 NC	3/8		4 3/8	3/8	2 3/4	9/16	3 1/16	3/8		1 7/16	2 1/16	1.4
EVR 4 NC		1/2	5	3/8	2 3/4	9/16	3 1/16	3/8		1 7/16	2 1/16	1.4
EVR 6 NC	3/8		4 3/8	3/8	2 3/4	9/16	3 1/16	3/8	2 3/16	1 7/16	2 1/16	1.4
EVR 6 NC	3/8		4 3/8	3/8	2 3/4	9/16	3 1/16	3/8	2 3/16	1 7/16	2 1/16	1.4
EVR 6 NC		1/2	5	3/8	2 3/4	9/16	3 1/16	3/8		1 7/16	2 1/16	1.4
EVR 6 NC		5/8	6 1/2	1/2	2 3/4	9/16	3 1/16	3/8		1 7/16	2 1/16	1.4
EVR 8 NC	3/8		4 5/8	3/8	2 3/4	9/16	3 1/16	3/8		1 7/16	2 1/16	1.4
EVR 8 NC		1/2	5	3/8	2 3/4	9/16	3 1/16	3/8		1 7/16	2 1/16	1.4
EVR 8 NC		5/8	6	1/2	2 3/4	9/16	3 1/16	3/8		1 7/16	2 1/16	1.4
EVR 10 NC	3/8		4 5/8	3/8	2 3/4	5/8	3 1/8	7/16		1 13/16	2 1/16	1.8
EVR 10 NC		1/2	5	3/8	2 3/4	5/8	3 1/8	7/16		1 13/16	2 1/16	1.8
EVR 10 NC		1/2	5	3/8	2 3/4	5/8	3 1/8	7/16	2 3/16	1 7/16	2 1/16	1.8
EVR 10 NC		5/8	6 5/16	1/2	2 3/4	5/8	3 1/8	7/16		1 13/16	2 1/16	1.8
EVR 15 NC	5/8		6 7/8	1/2	2 3/4	3/4	3 3/8	3/4		2 3/16	2 1/16	2.4
EVR 15 NC	5/8		6 7/8	1/2	2 3/4	3/4	3 3/8	3/4	2 1/8	2 3/16	2 1/16	2.4
EVR 15 NC		7/8	7 1/8	5/8	2 3/4	3/4	3 3/8	3/4		2 3/16	2 1/16	2.4
EVR 18 NC	7/8		7 1/8	5/8	2 3/4	3/4	3 3/8	3/4		2 3/16	2 1/16	2.4
EVR 18 NC		1 1/8	8 1/2	7/8	2 3/4	3/4	3 3/8	3/4		2 3/16	2 1/16	2.4
EVR 20 NC	7/8		7 1/2	5/8	2 3/4	25/32	3 9/16			2 13/16	2 1/16	3.4
EVR 20 NC	7/8		7 1/2	5/8	2 3/4	25/32	3 9/16		2 3/8	2 13/16	2 1/16	3.4
EVR 20 NC		1 1/8	8 1/2	7/8	2 3/4	25/32	3 9/16			2 13/16	2 1/16	3.4
EVR 22 NC	1 1/8		10 1/16	7/8	2 3/4	25/32	3 9/16			2 13/16	2 1/16	3.4
EVR 22 NC		1 3/8	11 1/16	1	2 3/4	25/32	3 9/16			2 13/16	2 1/16	3.4

¹⁾ H₂ for NO coils = H₂ for NC + 3/16 in.

Coil weight: 1 lb

Metric conversions: 1 in. = 25.4 mm

Dimensions and weights



Solder connections

Type	Connection		L in.	L ₂ in.	L ₅ in.	H ₁ in.	H ₂ in.	H ₄ in.	B in.	Weight with coil lbs
	normal size in.	oversize in.								
EVR 25	1 1/8		10 1/16	7/8	2 3/8	1 1/2	5 7/16	2 13/16	3 1/4	6.9
EVR 25		1 3/8	11 1/16	1	2 3/8	1 1/2	5 7/16	2 13/16	3 1/4	7.7
EVR 32	1 3/8		11 1/16	1	2 3/8	1 7/8	4 3/8	2 1/8	3 3/16	9.5
EVR 32		1 5/8	11 1/16	1 1/8	2 3/8	1 7/8	4 3/8	2 1/8	3 3/16	9.7
EVR 40	1 5/8		11 1/16	1 1/8	2 3/8	1 7/8	4 3/8	2 1/8	3 3/16	10.0
EVR 40		2 1/8	11 1/16	1 1/8	2 3/8	1 7/8	4 3/8	2 1/8	3 3/16	10.0

Coil weight: 1 lb

Metric conversions

1 in. = 25.4 mm

Spare parts, code nos.

Type	Seal kit	Service kit	Piston service kit	Pilot service kit
EVR 2	032F0220	032F0230		
EVR 3	032F0220	032F0230		
EVR 4	032F0221			
EVR 6	032F0221	032F0231		
EVR 8	032F0221	032F0231		
EVR 10	032F0222	032F0233		
EVR 15	032F0223	032F0235		
EVR 18	032F0223	032F0235		
EVR 20	032F0224	032F0237		
EVR 22	032F0224	032F0237		
EVR 25	032F3235			
EVR 32	042H0160		042H0176	042H0178
EVR 40	042H0160		042H0177	042H0178
EVR 6 NO	032F0221	032F0232		
EVR 10 NO	032F0222	032F0234		
EVR 15 NO	032F0223	032F0236		

Spare parts, contents

	Seal kit	Service kit	Piston service kit	Pilot service kit
	O-ring Gasket	Diaphragm assembly Armature assembly Rubber gasket Screws Torx key Snap fastener Nut	Piston assembly Plastic block Spring Piston ring Rubber gasket Snap fastener Nut	Armature tube assembly Snap fastener Armature Orifice Gaskets Nut